

NETL Carbon Capture Retrofit Analyses



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Solutions for Today | Options for Tomorrow



Systems Engineering & Analysis (SEA)

Teams and Scope



Energy Process Analysis

Energy Process Design, Analysis, and Cost Estimation

- Plant-level modeling, performance assessment
- Cost estimation for plant-level systems
- General plant-level technology evaluation and support



Energy Systems Analysis

Resource Availability and Cost Modeling

- CO₂ storage (saline and EOR)
 - Fossil fuel extraction
 - Rare earth elements
 - General subsurface technology evaluation and support
- Grid modeling and analysis

Environmental Life Cycle Analysis



Process Systems Engineering Research

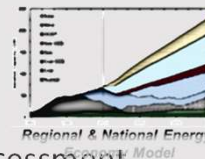
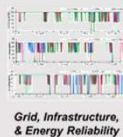
- Process synthesis, design, optimization, intensification
- Steady state and dynamic process model development
- Uncertainty quantification
- Advanced process control

Design, optimization, and modeling framework to be expanded to all SEA “systems”

Energy Markets Analysis

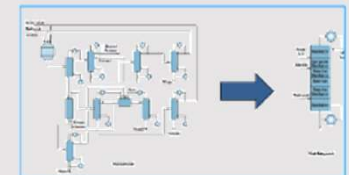
Energy Economy Modeling and Impact Assessment

- Enhanced fossil energy representation
- Multi-model scenario/policy analysis
- Infrastructure, energy-water

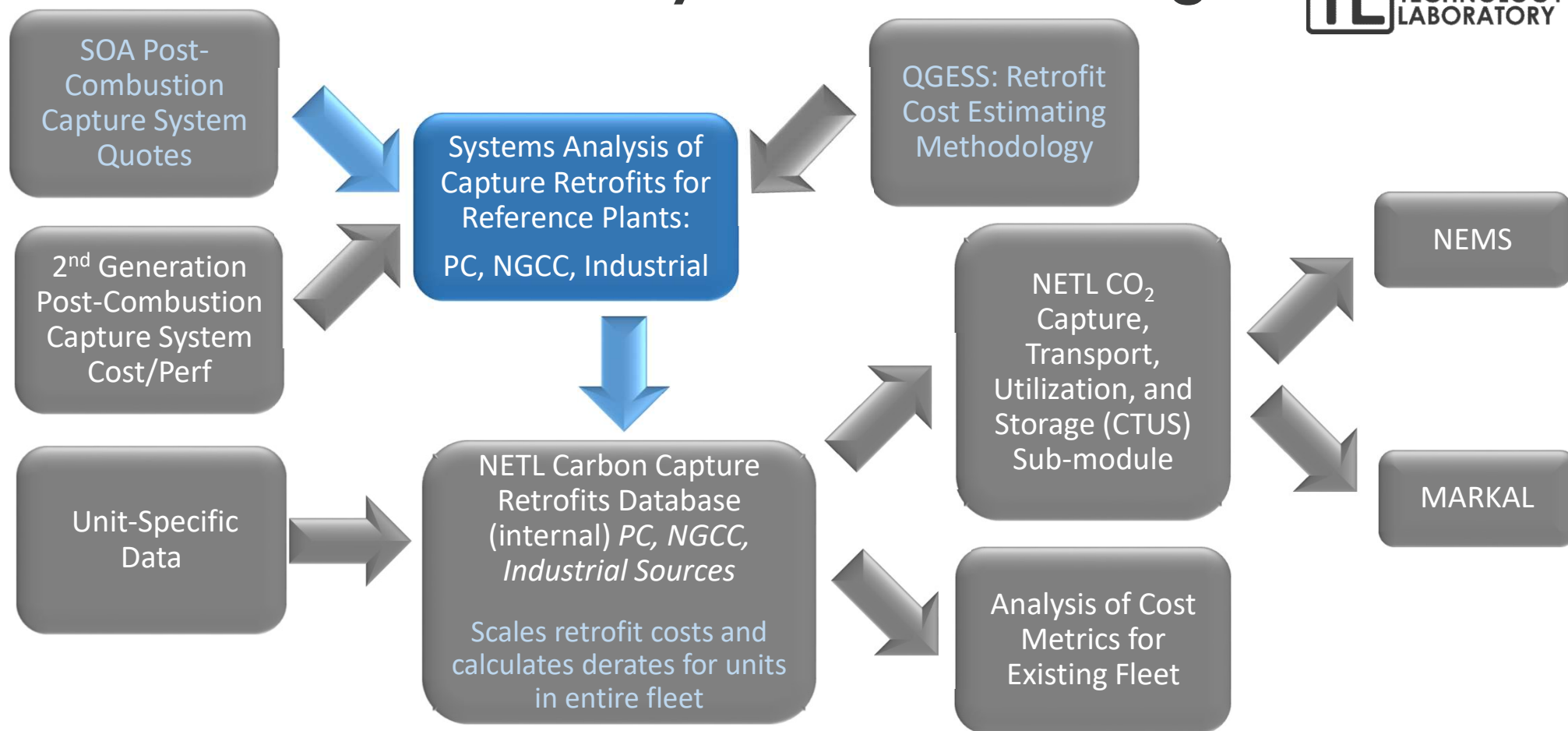


- Economic impact assessment
- General regulatory, market and financial expertise

Advanced Energy Systems through Process Systems Engineering



NETL CCS Retrofit Analysis and Modeling



Why Analyze CCS Retrofits?



- Evaluate scenarios where there is a price on CO₂ emissions
- Consider economic feasibility of power plants or industrial sources that sell CO₂ for Enhanced Oil Recovery (EOR)
- Analyze benefits of CO₂ capture R&D on existing fleet of power plants and industrial sources

Carbon Capture Retrofit Modeling Overview



- 264 GW of existing coal and 242 GW of existing NGCC capacity in U.S.*
- CO₂ also available for capture from industrial sources; publicly available information from EPA's Greenhouse Gas Reporting Program
- Access to heat rate, nameplate capacity, O&M costs, CO₂ emissions, pollution controls, online date, other relevant data from which to estimate CCS retrofit costs
- Based on similar results of NETL studies, employ a factored approach to existing fleet to estimate cost, performance impact of CCS retrofits
- Determine sensitivity to capacity factor or financing assumptions, evaluate impact of advanced CCS R&D, assess benefits of EOR opportunities

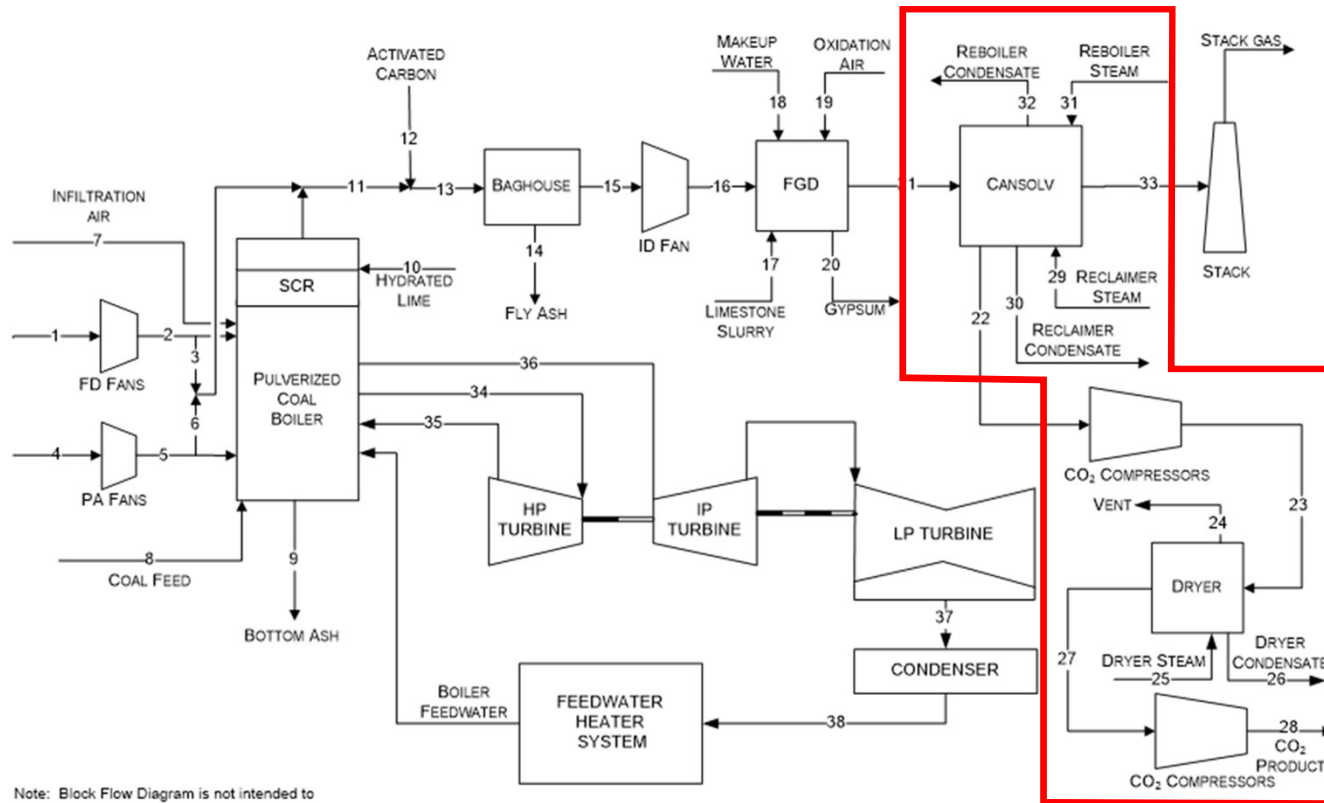
CO₂ Capture Retrofit – Existing Coal Units



- Study in progress – Carbon Capture Retrofit of Existing Coal Units
- Expected publication late 2017



Subcritical Pulverized Coal with CO₂ Capture

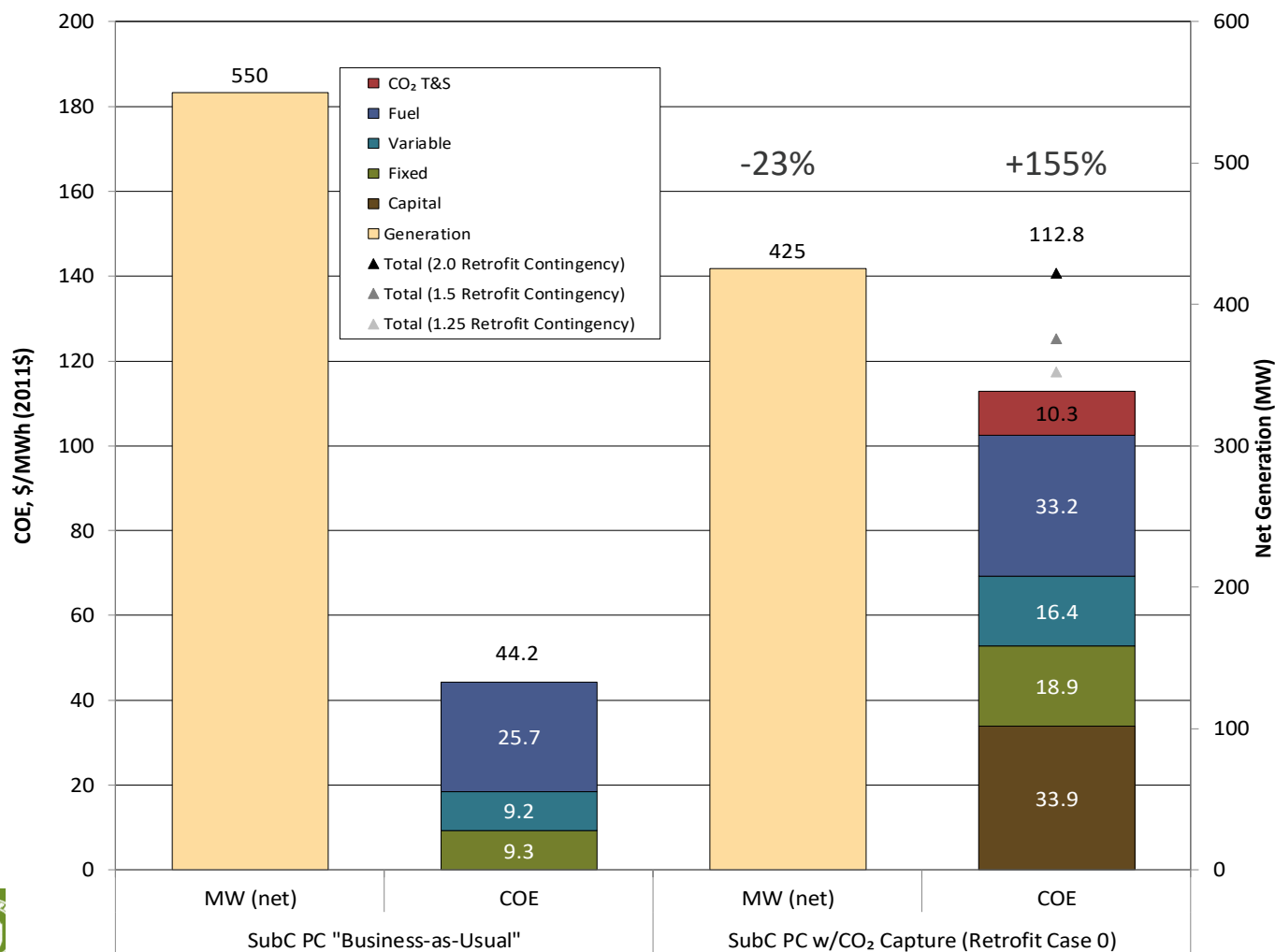


Pulverized Coal Retrofit Study Assumptions



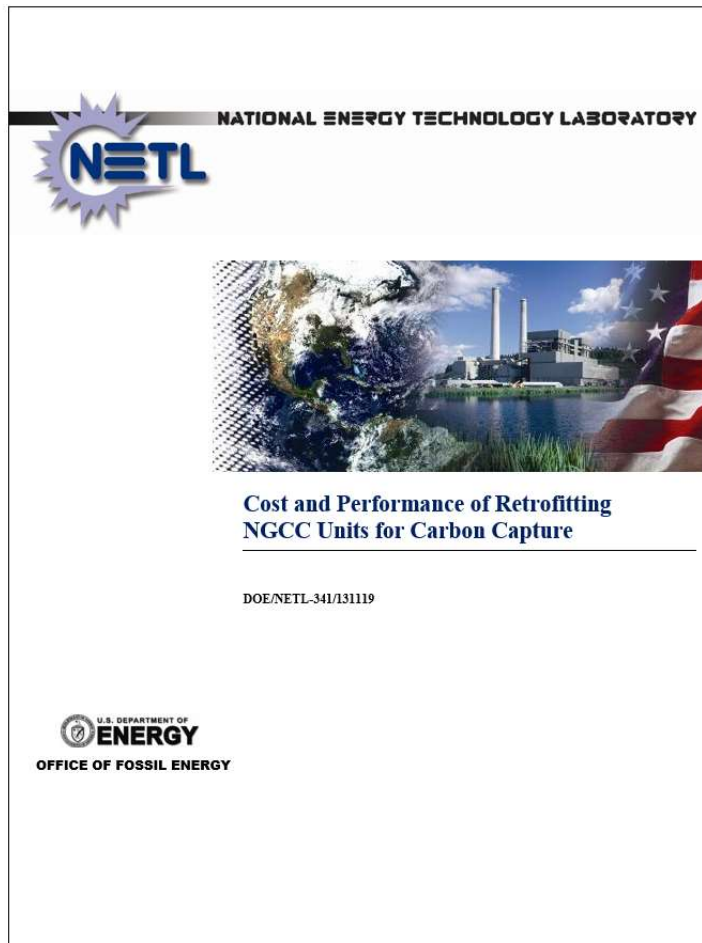
Steam Conditions (psig/°F/°F)	2,400/1,050/1,050
Coal	Illinois #6 Bituminous
Condenser Pressure	2" Hg
SO ₂ Control	Wet FGD
NO _x Control	Low NO _x burner with overfire air, SCR
Particulate Control	Fabric filter
Hg Control	ACI
CO ₂ Control	Cansolv
CO ₂ Capture Efficiency	90%
CO ₂ Fate	Offsite saline storage
CO ₂ Pipeline Transport Distance	100 km

Subcritical PC Retrofit Results



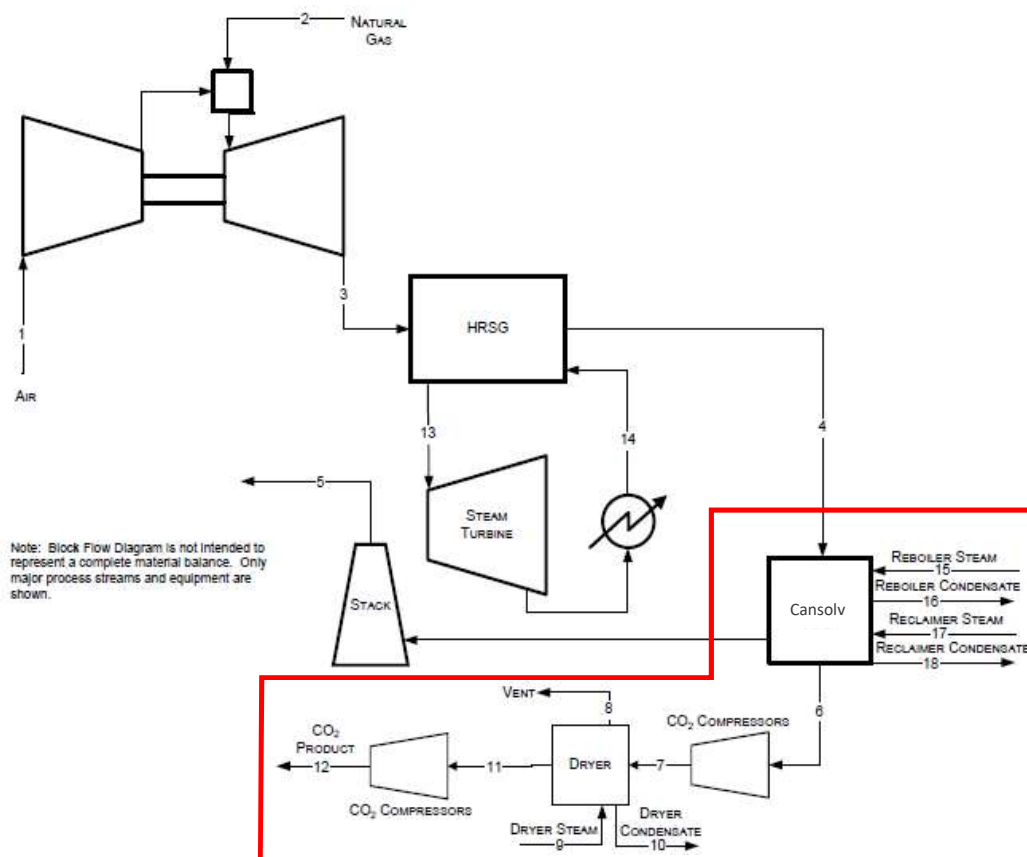
Retrofit Capex	\$726,600,000
Heat Rate (pre retrofit)	8,740 Btu/kWh
Heat Rate (post retrofit)	11,300 Btu/kWh
CO ₂ Capture Rate	240,218 Lb CO ₂ /hr
Energy Penalty	≈0.14 kWh/Lb CO ₂ captured
Incremental O&M	\$18.8/MWh

CO₂ Capture Retrofit – Existing NGCC Units



- Study in progress – Carbon Capture Retrofit of Existing NGCC Units
- Expected publication late 2017

NGCC with CO₂ Capture

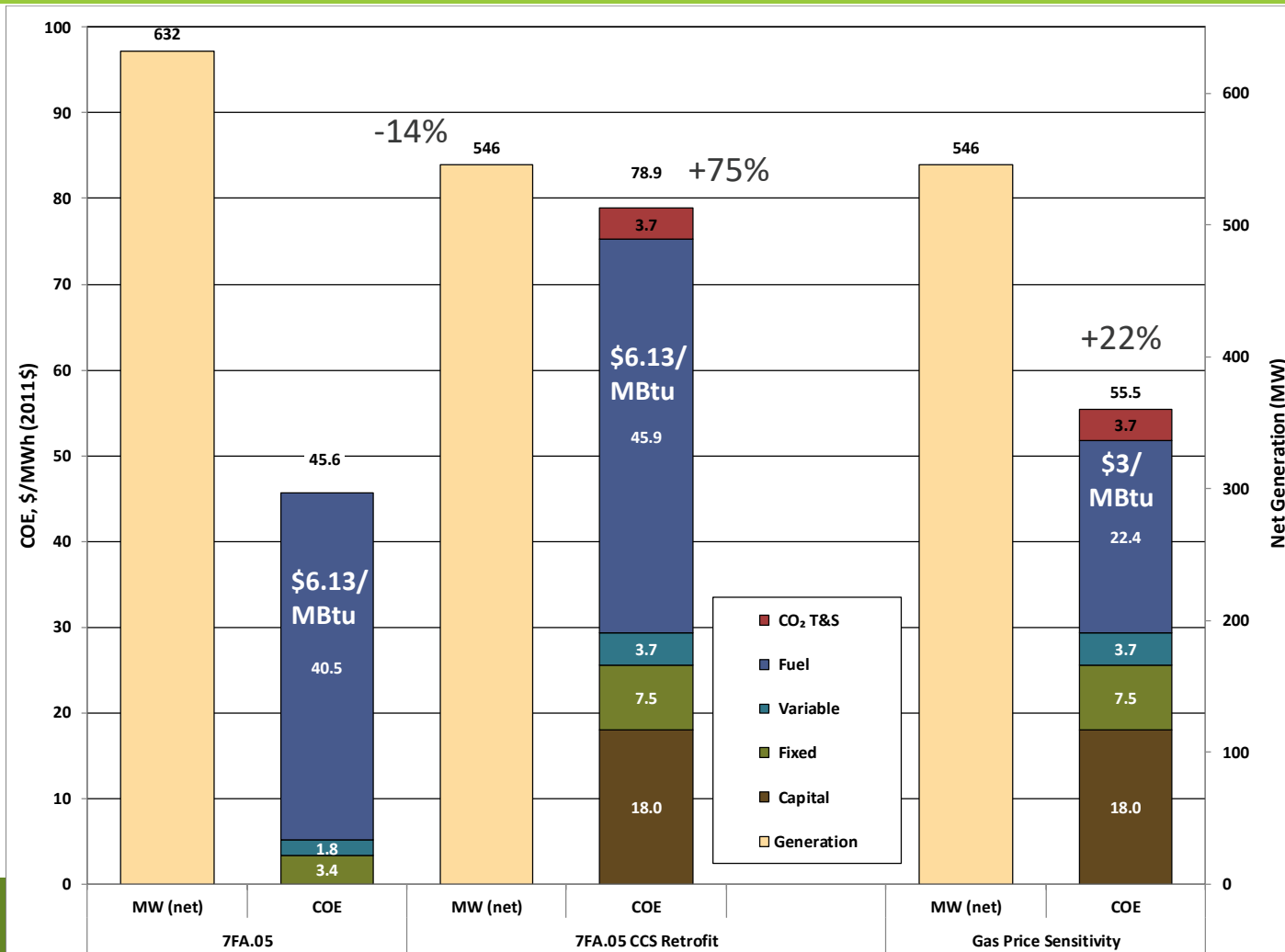


NGCC CCS Retrofit Study Assumptions



Steam Conditions (psig/°F/°F)	2,400/1,050/1,050
Gas Turbine	2 x GEE 7FA
Turbine Inlet Temperature	2,479 °F
CO ₂ Control	Cansolv
CO ₂ Capture Efficiency	90%
CO ₂ Fate	Offsite saline storage
CO ₂ Pipeline Transport Distance	100 km

NGCC Retrofit Results



- NGCC cost of electricity highly sensitive to gas price!

Retrofit Capex	\$647,300,000
Heat Rate (pre retrofit)	6,629 Btu/kWh
Heat Rate (post retrofit)	7,466 Btu/kWh
CO ₂ Capture Rate	445,486 Lb CO ₂ /hr
Energy Penalty	≈0.19 kWh/Lb CO ₂ captured
Incremental O&M	\$6.15/MWh

CO₂ Capture Retrofit Difficulty Factor



- Power plant retrofits typically space constrained
- A retrofit “difficulty factor” can be applied to capital costs to reflect site-specific challenges
- Factor only applied to capex, so impact on total cost of electricity can be easily assessed
- NETL Quality Guidelines for Energy System Studies – “Estimating Plant Costs Using Retrofit Difficulty Factors*”

Incidental Retrofit Project Costs



- Existing coal units may require other environmental upgrades when adding CO₂ capture equipment
- Cost for NO_x (SCR), SO₂ (FGD) upgrades should be considered to reflect all-in project cost
- CCS retrofit is a long-term bet on plant viability, may also want to consider cost for conversion from wet to dry cooling in certain regions (50% water consumption increase when capturing 90% CO₂)

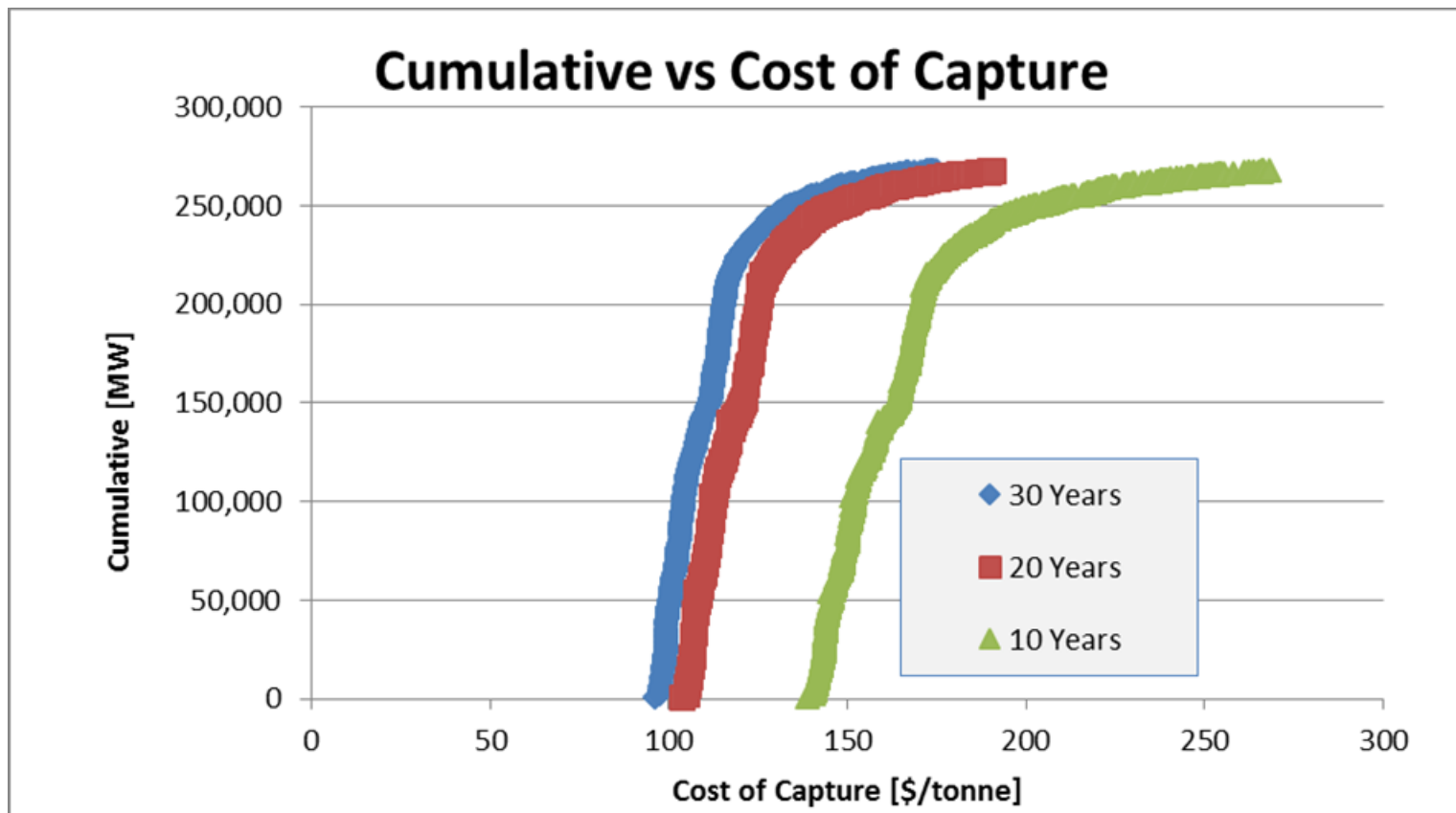
Retrofit Financing Considerations



- NETL studies typically assume 30 year economic life (reflected in capital charge factor)
- What is expected remaining useful life of an existing coal unit retrofitted with CCS? Majority of existing coal fleet built in the 1970's.
- Financing assumptions needed to reflect scenarios shorter than 30-year default

Retrofit Financing Considerations

Impact of economic life on cost results



Opportunity Cost of CCS Retrofits



- In addition to incremental capital, O&M costs, lost power sales revenue due to plant derate needs to be considered
- Useful way to determine minimum CO₂ EOR sale price to justify CCS retrofit

$$\begin{array}{l} \text{Annualized Capital} \\ \text{and Incremental O\&M} \\ \text{Costs for Retrofit} \end{array} + \begin{array}{l} \text{Annual Revenues} \\ \text{Foregone Due to Lost} \\ \text{Generation (Derate)} \end{array} \leq \begin{array}{l} \text{Annual Revenues} \\ \text{from Sale of} \\ \text{Captured CO}_2 \end{array}$$

Cost Scaling Methodology



- Capital costs for CO₂ capture equipment scaled from reference plant costs, based on amount of CO₂ removed; do NOT scale based on plant output
- Operation and maintenance costs scaled from reference plant costs, based on total plant capital cost
- Retrofit difficulty factor can be applied to capital costs
- Year dollar basis can show historic market fluctuations
- NETL Quality Guidelines for Energy System Studies – “Capital Cost Scaling Methodology*”

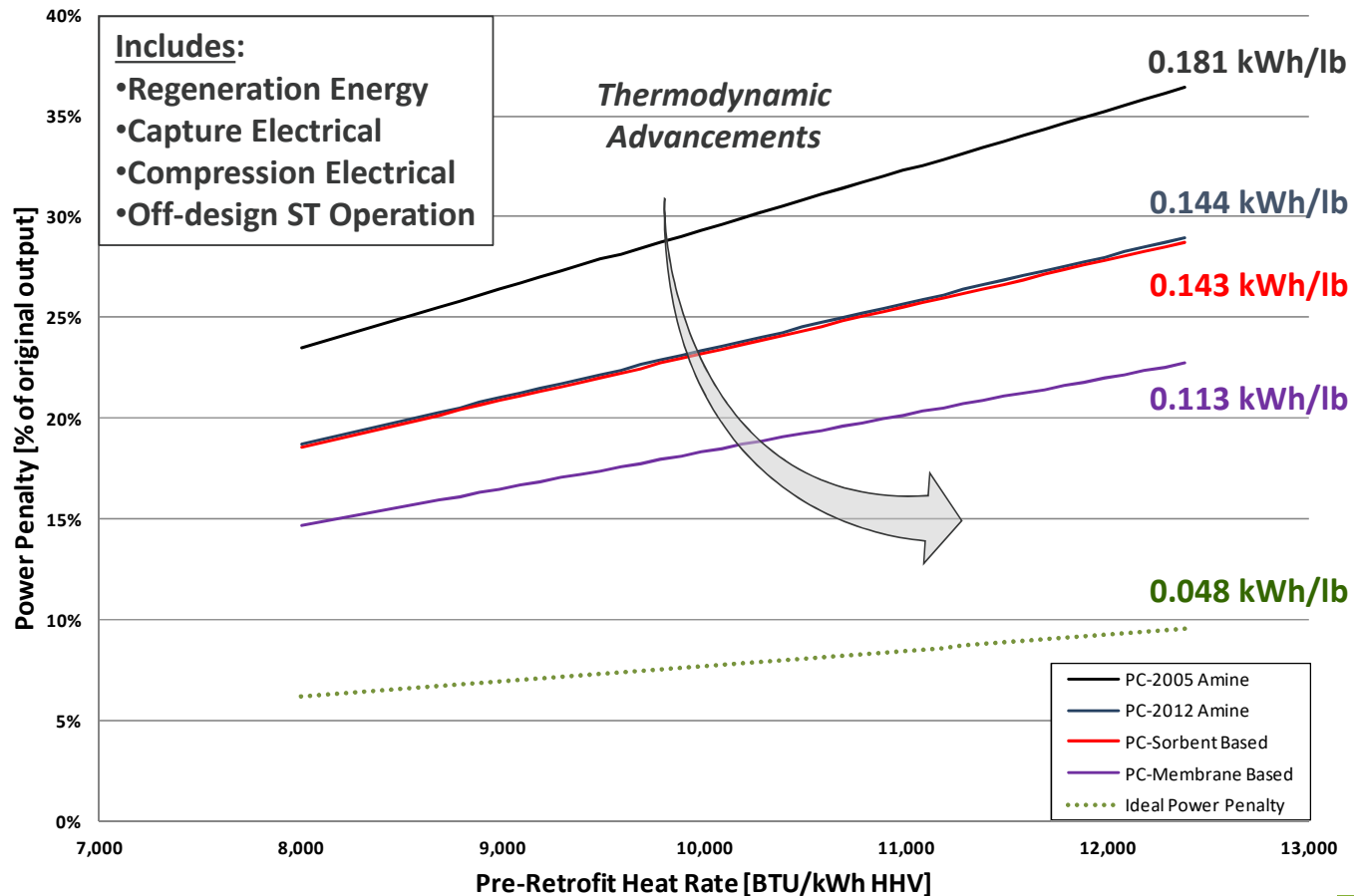
Parasitic Power Load Scaling Methodology



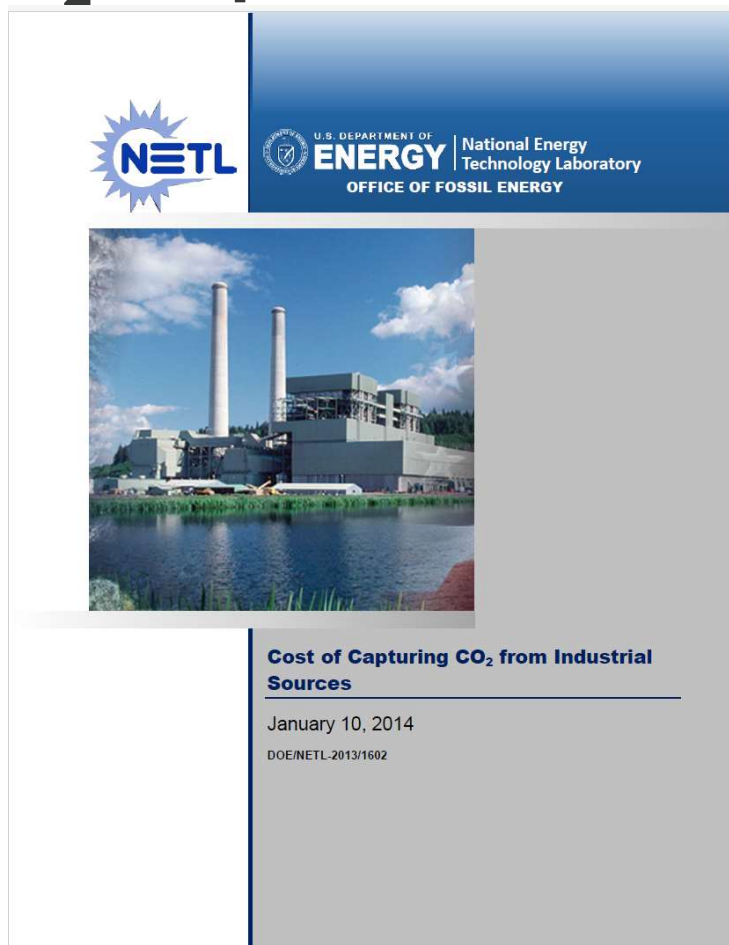
- Parasitic power load for retrofitted units can be scaled from reference cases, based on CO₂ captured (Lb/hr); do NOT simply add a % derate of net power
- Energy Penalty (kWh/Lb CO₂) =
$$\frac{MWh_{non-capture} - MWh_{capture}}{CO_2 \text{ captured } \left(\frac{lb}{year} @ 100\% CF \right)}$$
- Allowances for other environmental (or other) upgrades (SCR, FGD, dry cooling) can also be made as needed

Net Derate Projections

Net Output Penalties of CCS Retrofits



CO₂ Capture Retrofit – Industrial Sources



- CO₂ Capture from Industrial Sources* – Public Report

Industrial Source CO₂ Capture



- Does the industrial source represent a target rich opportunity?
- CO₂ concentration in stack gas is a consideration
- Do industrial source capture conditions (temperature, pollutant levels) align with capabilities of current CO₂ capture technologies?

Industrial Source CO₂ Capture

Industrial Process	Reference Plant Capacity	CO ₂ Source Stream	CO ₂ to Product Ratio (tonne CO ₂ /tonne Product)	Source Stream CO ₂ Concentration (mol%)	Source Stream CO ₂ Partial Pressure (psia)	CO ₂ Available for Capture (M tonnes CO ₂ /year)		Breakeven Cost of Capturing CO ₂ (\$/tonne CO ₂)
						Reference Plant	All U.S. sources	
High Purity Sources								
Ethanol	50 M gal/year	Distillation gas	0.96	100	18.4	0.14	40	30
Ammonia	907,000 tonnes/year	Stripping vent	1.9	99	22.8	0.458	6	27
Natural Gas Processing	500 MMscf/d	CO ₂ vent	N/A ¹	99	23.3	0.649	27	18
Ethylene Oxide	364,500 tonnes/year	AGR product stream	0.33	100	43.5	0.122	1	25
Coal-to-Liquids (CTL)	50,000 bbl/d	AGR product stream	N/A ²	100	265	8.74	-	9
Gas-to-Liquids (GTL)	50,000 bbl/d	AGR product stream	N/A ²	100	265	1.86	-	9
Low Purity Sources								
Refinery Hydrogen	59,000 tonnes/year	PSA tail gas	10.5	44.5	8.9	0.274	68	118
Iron/Steel	2.54 M tonnes/year	Plant Total	2.2	N/A	N/A	3.9	49	99
		COG PPS		23.2	3.4	2.75		99
		COG/BFG ³		26.4	3.9	1.16		101
Cement SCR/FGD Sensitivity	992,500 tonnes/year	Kiln Off-gas	1.2	22.4	3.3	1.14	80	100
Coal-fired power plants	550 MW	Flue Gas	NA	13.5	2.0	4.13	2,545 ⁴	77 ⁵⁶

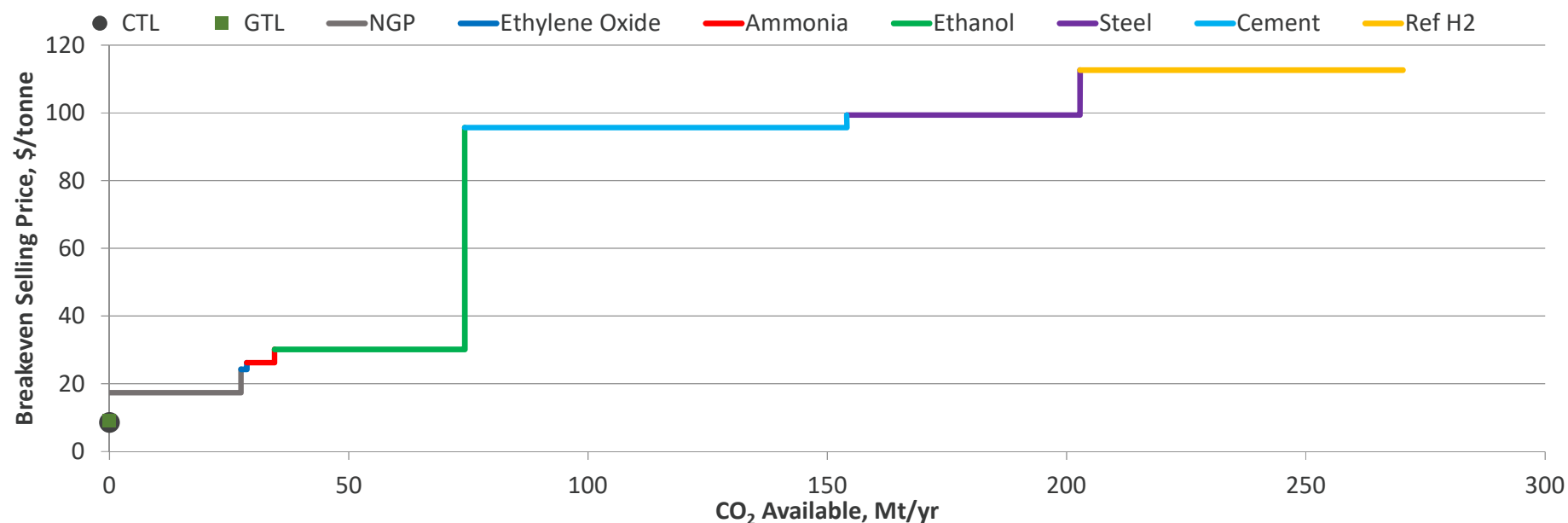
High/Low CO₂ Purity Results Comparison



	Refinery Hydrogen (Low CO ₂ Purity)	Ethylene Oxide (High CO ₂ Purity)
Source Stream CO ₂ Purity	44.5 mol %	100 mol %
	Breakeven Cost, \$/tonne CO ₂	Breakeven Cost, \$/tonne CO ₂
Capital Charges	41.37	9.85
Fixed O&M	12.57	3.47
Variable O&M	18.86	5.20
Consumables	2.71	0.27
Purchased Power	11.24	5.49
Purchased Natural Gas	25.88	0.00
Total Breakeven Cost	112.64	24.28

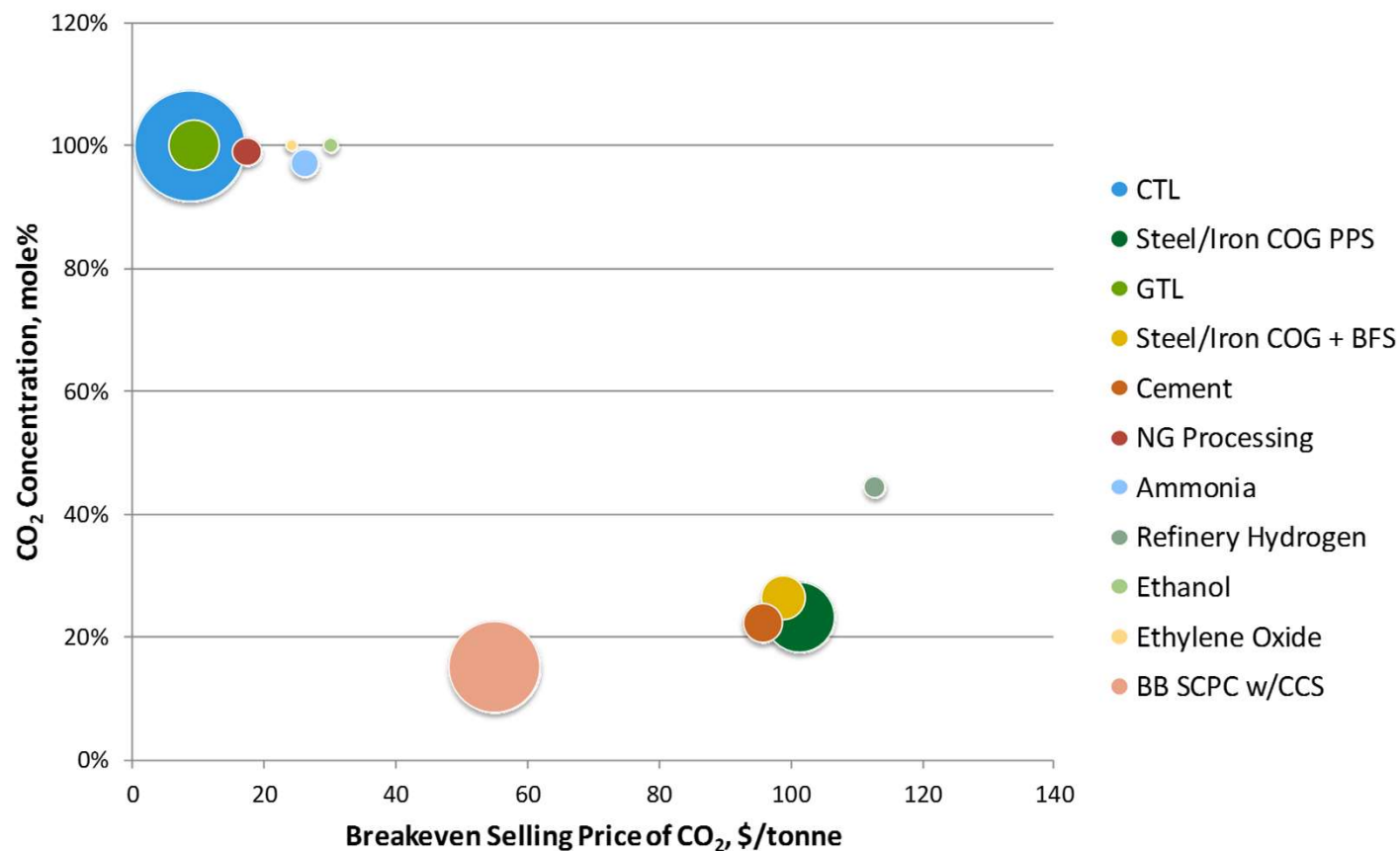
Capturing CO₂ from Industrial Sources

Incremental CO₂ Supply versus Breakeven Selling Price



Capturing CO₂ from Industrial Sources

Breakeven Selling Price as a Function of CO₂ Concentration



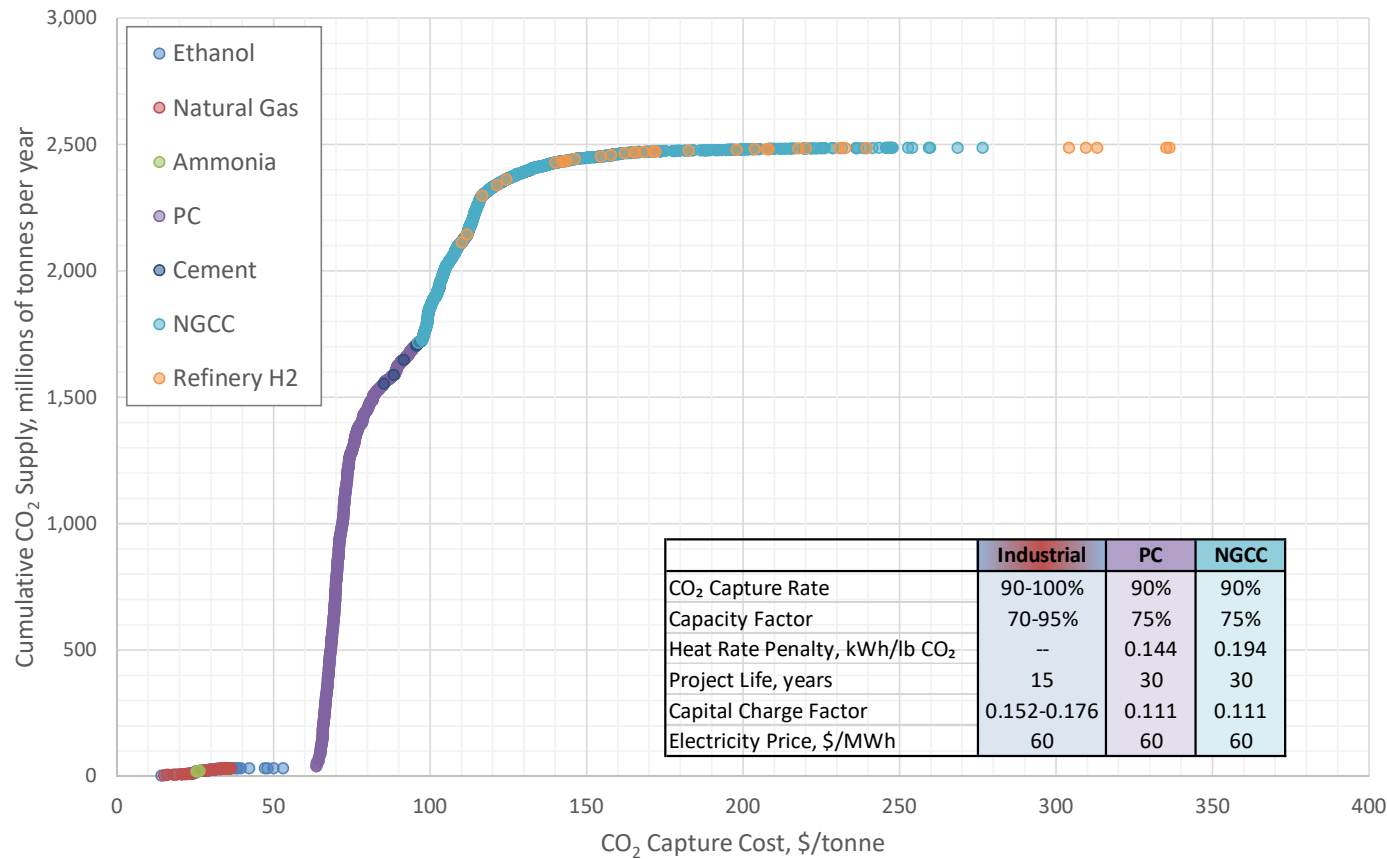
Industrial Source Retrofit Methodology



- Facility data for industrial sources based on EPA's Greenhouse Gas Reporting Program¹ and FLIGHT data²
- Plant capacity in report based on typical sizes, cost and performance post-retrofit based on source report, and applied using a scaled approach
- Key parameters of interest include payback period, financing structure, supplemental power or natural gas price

Cumulative CO₂ Supply

Large capacity available, at increasing cost of capture



Future Work



- Finalization of existing coal, NGCC retrofit source reports
- Continued development of internal version of retrofit model
- Development of public version of retrofit model

Contact Information



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Thanks to everyone involved in the development of this effort!!



Thank You.

